Effect of the Cyclopentadienyl Fragment on Monomer Reactivities and Monomer Sequence Distributions in Ethylene/α-Olefin Copolymerization by a Nonbridged (Cyclopentadienyl)(aryloxy)titanium(IV) Complex–MAO Catalyst System

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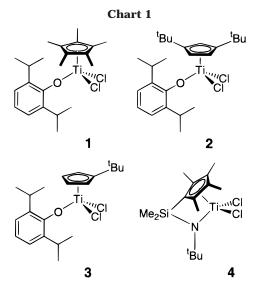
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Introduction. Olefin polymerization by homogeneous transition metal catalysis has been one of the most attractive subjects in the fields of both organometallic chemistry and polymer chemistry. There have thus been many reports concerning this topic especially using group 4B transition metal complexes. We have recently reported that $Cp^*TiCl_2(O-2,6^{-i}Pr_2C_6H_3)$ ($Cp^* = C_5Me_5$ 1) exhibited remarkable catalytic activity for ethylene homopolymerization as well as for ethylene/1-butene copolymerization in the presence of MAO (methylaluminoxane)² and that the copolymerization did not proceed in a random manner. The latter feature is completely different from that observed by hybrid "halfmetallocene" type $[Me_2Si(C_5Me_4)(N^tBu)]\check{T}iC\check{l}_2$ (4) as well as by an ordinary metallocene-type catalyst. ^{1a-f,3} Since the control of the monomer sequence in ethylene/ α -olefin copolymers, which are widely used commercially, has been an unsolved problem in this research field, 4,5 we thus began to investigate the different behaviors in more detail. In this paper, we wish to introduce our examined results concerning the effect of the cyclopentadienyl fragment on monomer reactivity ratios and the microstructure of poly(ethylene-*co*-1-hexene)s in these polymerizations.

Results and Discussion. On the basis of the preliminary results concerning the effects of substituent of the cyclopentadienyl group on ethylene, 1-hexene, and 1-octene homopolymerizations, 7 we chose three different catalysts, $Cp^*TiCl_2(O-2,6-^iPr_2C_6H_3)$ (1), $(1,3-^iBu_2C_5H_3)$ - $TiCl_2(O-2,6-^iPr_2C_6H_3)$ (2), and $(^iBuC_5H_4)TiCl_2(O-2,6-^iPr_2C_6H_3)$ (3) (Chart 1), because these complexes, especially 2, showed different catalytic activities in these homopolymerizations. 4 was chosen as the reference. The results are summarized in Table 1.8

It was revealed that **1** exhibited a remarkable catalytic activity under optimal conditions and that the activity was much higher than **4** in the presence of MAO which was prepared from commercially available MAO (PMAO-S) by removing toluene and the excess AlMe₃ in vacuo. The resultant copolymers possessed relatively high molecular weights, unimodal molecular weight distributions ($M_w = (31.7-45.5) \times 10^4$; $M_w/M_n = 1.77-1.98$), and relatively high 1-hexene contents (24.2–42.5 mol %) which were of the same level as those obtained by **4**.9 The observed catalytic activity decreased when the polymerization was performed at 15 °C, but the rate was unchanged between 25 and 50 °C (69.4, 181, 179,



and 176 \times 10³ kg of polymer/(mol of Ti h) at 15, 25, 40, and 50 °C, respectively). ¹⁰ The observed catalytic activity also decreased at a low Al/Ti molar ratio, but the $M_{\rm w}$ values of the resultant copolymers were unchanged under different Al/Ti molar ratios (139, 179, and 189 \times 10³ kg of polymer/(mol of Ti h); $M_{\rm w}=33.4$, 33.2, and 32.1 \times 10⁴ at Al/Ti = 20 000, 30 000, and 50 000, respectively). ¹⁰

It is important to note that the 1-hexene content in the resultant copolymer depends strongly upon the substituent of Cp' group under the same conditions. The complex **3** exhibited the highest level of 1-hexene incorporation among these complexes (example: 42.5, 37.5, and 59.0 mol % by **1**, **2**, and **3**, respectively, at ethylene 5 atm and 1-hexene 1.45 mmol/mL), indicating that the nature of cyclopentadienyl fragment affects the relative rate of monomer coordination or insertion.

Triad sequence distributions in the resultant poly-(ethylene-co-1-hexene)s determined by ¹³C NMR spectra¹¹ and the monomer reactivity ratios¹² are summarized in Table 2. The sequence distributions of copolymers shows that the contents of EHE and HHE + EHH sequences and the resultant $r_E r_H$ values (r_E and r_H are the monomer reactivity ratios of ethylene and 1-hexene, respectively) by 1-3 are significantly different from that by 4 under the same conditions. The monomer reactivity ratios in the copolymerimerization with 4 are consistent with those reported previously^{1d,e,3} and a little larger than those obtained by 1-3. The difference might reflect the different structure or different electronic structure either of the catalytically active species. In addition, $r_{\rm E}$, $r_{\rm H}$, and $r_{\rm E}r_{\rm H}$ values were not strongly affected either by the reaction temperature or by the Al/Ti molar ratio under the present conditions.¹³ These are in contrast with those in copolymerizations by ordinary metallocene catalysts.14

Noteworthy is that the sequence distributions as well as their $r_{\rm E}$, $r_{\rm H}$, and $r_{\rm E}r_{\rm H}$ values in the copolymerizations by **1–3** were strongly affected by the nature of the cyclopentadienyl group. This result should be very interesting for the first example of that the substitutents in cyclopentadienyl group *directly* control the monomer reactivity ratios and sequence distributions in ethylene/1-hexene copolymerization.

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Table 1. Copolymerization of Ethylene with 1-Hexene by a $Cp'TiCl_2(O-2,6-^{i}Pr_2C_6H_3)$ –MAO Catalyst System $[Cp'=Cp^*\ (1), 1,3-^{i}Bu_2C_5H_3\ (2), and ^{i}BuC_5H_4\ (3)]^a$

run no.	complex (concn/µmol)	temp/°C	Al/Ti ^b	ethylene/atm	1-hexene concn ^c	activity $^d/\times 10^{-3}$	1-hexene ^e /mol %	$M_{\rm w} / \times 10^{-4} {\rm f}$	$M_{\rm w}/M_{\rm n}$ f
	1 (0.07)	40	30 000	5	1.45	179	42.5	31.7	1.77
2				5	1.45	176	43.4	33.2	1.77
	1 (0.07)	40	30 000						
3	1 (0.07)	40	30 000	5	1.22^{g}	198	36.6	33.8	1.83
4	1 (0.07)	40	30 000	7	1.45	263	38.1	33.7	1.87
5	1 (0.10)	40	30 000	5	1.09	79.5	40.3	32.0	1.88
6	1 (0.10)	40	30 000	7	1.09	120	36.0	33.4	1.73
7	1 (0.08)	40	25 000	5	0.73	83.2	28.6	38.2	1.80
8	1 (0.08)	40	25 000	7	0.73	103	24.2	45.5	1.98
9	$4^{h}(0.60)$	40	5000	5	0.73	9.49	30.0	74.5	2.05
10	2 (0.45)	40	6500	5	1.45	4.70	37.5	10.3	1.84
11	2 (0.45)	40	6500	7	1.45	6.85	33.9	12.4	1.78
12	2 (0.30)	40	9000	5	0.73	11.3	27.0	19.7	1.82
13	2 (0.30)	40	9000	7	0.73	17.5	23.5	14.5	1.71
14	3 (0.75)	40	4000	5	1.45	8.79	59.0	10.4	1.58
15	3 (0.75)	40	4000	7	1.45	15.0	41.4	13.0	1.60
16	3 (0.60)	40	5000	5	0.73	6.41	32.0	11.4	1.99
17	3 (0.60)	40	3300	7	0.73	14.2	26.9	12.7	1.60

 a Reaction conditions: toluene + 1-hexene, total 55 mL (runs 10–13, 66 mL); MAO white solid, prepared by removing toluene and AlMe3; time, 6 min (runs 12, 13, and 17, 8 min; runs 15 and 16, 5 min); 100 mL scale autoclave. b Molar ratio of Al/Ti. c 1-Hexene concentration, mmol/mL. d kg of polymer/(mol of Ti h). e 1-Hexene content in copolymer determined by $^{13}\mathrm{C}$ NMR spectra. f GPC in o-dichlorobenzene vs polystyrene standard. g 1-Octene used in place of 1-hexene. h [Me2Si(C5Me4)(N r Bu)]TiCl2 as catalyst.

Table 2. Monomer Sequence Distirbution of Poly(ethylene-co-1-hexene)s^a

			triad sequence distribution ^c /%						\mathbf{diad}^d					
run no.	complex	1-hexene ^b /mol %	EEE	EEH + HEE	HEH	EHE	HHE + EHH	ННН	EE	EH + HE	НН	$r_{\rm E}r_{\rm H}$ e	$r_{\rm E}$ f	$r_{\rm H}$ f
7	1	28.6	31.1	31.3	8.9	21.5	6.8	0.4	46.8	49.5	3.7	0.28	2.70	0.10
8	1	24.2	40.0	29.6	5.8	19.4	4.6	0.6	55.1	42.5	2.4	0.29	2.64	0.11
11	2	33.9	26.0	29.7	10.4	20.5	12.0	1.4	40.9	51.7	7.4	0.45	3.23	0.14
12	2	27.0	34.6	31.2	7.1	18.4	7.8	0.9	50.3	45.0	4.8	0.48	3.19	0.15
15	3	32.0	27.6	31.4	9.0	20.1	10.9	1.0	43.3	50.2	6.5	0.45	2.46	0.18
17	3	26.9	35.9	31.1	6.2	19.2	7.3	0.4	51.4	44.6	4.0	0.41	2.35	0.18
9	4	30.0	35.5	28.6	5.9	14.2	14.4	1.4	49.8	41.6	8.6	0.99	3.42	0.29

 a For detailed polymerization conditions, see Table 1. b 1-Hexene content in copolymer determined by ^{13}C NMR spectra. c Determined by ^{13}C NMR spectra. d [EE] = [EEE] + $^1/_2$ [EEH + HEE], [EH] = [HEH] + [EHE] + $^1/_2$ [EEH + HEE] + [HHE + EHH]}, [HH] = [HHH] + $^1/_2$ [HHE + EHH]. e r_Er_H = 4[EE][HH]/[EH + HE]². f r_e = [H]₀/[E]₀ × 2[EE]/[EH + HE], n_h = [E]₀/[H]₀ × 2[HH]/[EH + HE], [E]₀ and [H]₀ are the initial monomer concentrations.

We believe that the high extent of α -olefin incorporation by **1**-**3**, despite the rather wide bond angles^{2b} of Cp-Ti-O in **1** (120.5°) and **2** (119.3°) than that of

Cp-Ti-N in **4** (107.6°), ¹⁵ would be due to the rotational flexibility of these complexes. In addition, the influence of the substituted cyclopentadienyl group on the mono-

mer reactivity ratios and the sequence distributions would also be due to its easy internal rotation, facilitating coordination or insertion of higher olefins (Scheme 1). We are currently studying the mechanism of polymerization in more detail.

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Supporting Information Available: Text giving experimental details of general polymerization procedures in the presence of MAO, figures showing $^1{\rm H}$ and $^{13}{\rm C}$ NMR spectra of poly(ethylene-co-1-hexene)s and poly(ethylene-co-1-octene) prepared by **1–3** or [Me₂Si(C₅Me₄)(N^tBu)]TiCl₂ (shown in Table 2), and tables giving polymerization results concerning the effects of reaction temperature and the Al/Ti molar ratio (total 12 pages). This material is available free of charge via the Internet at http://pubs.acs.org.

References and Notes

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- To control the 1-hexene conversion less than 10%, these copolymerizations were terminated at 5-8 min. For more experimental details, see the Supporting Information.
- Molecular weight and molecular weight distribution of the resultant copolymers were measured by gel permeation chromatography (Tosoh HLC 8121GPC/HT) with a polystyrene gel column (TSK gel GMH_{HR}-H HT \times 2) at 140 °C using o-dichlorobenzene containing 0.05 w/v % 2,6-di-tert-butylp-cresol as solvent. The molecular weight was calculated by a standard procedure based on the calibration with standard polystyrene samples.
- (10) These copolymerizations were performed under the same conditions as in run 1, except the reaction temparature or Al/Ti molar ratio. For details, see the Supporting Information.
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